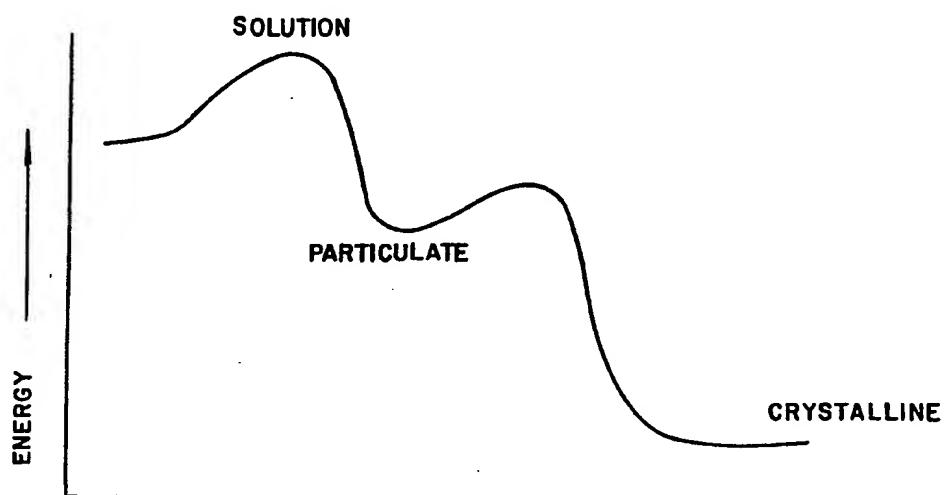




INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(51) International Patent Classification 5 : C01F 7/34, A61J 3/02		A1	(11) International Publication Number: WO 92/03380 (43) International Publication Date: 5 March 1992 (05.03.92)
(21) International Application Number: PCT/US90/04735 (22) International Filing Date: 21 August 1990 (21.08.90)		(81) Designated States: AT (European patent), AU, BE (European patent), CA, CH (European patent), DE (European patent), DK (European patent), ES (European patent), FI, FR (European patent), GB (European patent), IT (European patent), JP, KR, LU (European patent), NL (European patent), NO, SE (European patent).	
(71) Applicant: THE UNIVERSITY OF ROCHESTER (US/US); Office of Research and Project Administration, 30 Administration Building, Rochester, NY 14627 (US).		Published <i>With international search report.</i>	
(72) Inventors: VIOLANTE, Michael, R. ; 688 Surrey Hill Way, Rochester, NY 14623 (US). FISCHER, Harry, W. ; 110 Old Stonefield Way, Pittsford, NY 14534 (US).			
(74) Agents: HUETTNER, Richard, A. et al.; Kenyon & Kenyon, One Broadway, New York, NY 10004 (US).			

(54) Title: METHOD FOR MAKING UNIFORMLY-SIZED PARTICLES FROM INSOLUBLE COMPOUNDS



(57) Abstract

The invention involves a method for making uniformly sized particles from solid compounds. First, a suitable solid compound is dissolved in a suitable solvent. Then, a precipitating liquid is infused, precipitating non-aggregated particles with substantially uniform mean diameter. The particles are then separated from the solvent. Depending on the solid compound and the desired particle size, the parameters of temperature, ratio of non-solvent to solvent, infusion rate, stir rate, and volume can be varied according to the invention. The precipitating liquid may be aqueous or non-aqueous, depending upon the relative solubility of the compound and the desired suspending vehicle.

FOR THE PURPOSES OF INFORMATION ONLY

Codes used to identify States party to the PCT on the front pages of pamphlets publishing international applications under the PCT.

AT	Austria	ES	Spain	MC	Madagascar
AU	Australia	FI	Finland	ML	Mali
BB	Barbados	FR	France	MN	Mongolia
BE	Belgium	GA	Gabon	MR	Mauritania
BF	Burkina Faso	GB	United Kingdom	MW	Malawi
BG	Bulgaria	GN	Guinea	NL	Netherlands
BJ	Benin	GR	Greece	NO	Norway
BR	Brazil	HU	Hungary	PL	Poland
CA	Canada	IT	Italy	RO	Romania
CF	Central African Republic	JP	Japan	SD	Sudan
CG	Congo	KP	Democratic People's Republic of Korea	SE	Sweden
CH	Switzerland	KR	Republic of Korea	SN	Senegal
CI	Côte d'Ivoire	LJ	Liechtenstein	SU ⁺	Soviet Union
CM	Cameroon	LK	Sri Lanka	TD	Chad
CS	Czechoslovakia	LU	Luxembourg	TC	Togo
DE*	Germany	MC	Monaco	US	United States of America
DK	Denmark				

+ Any designation of "SU" has effect in the Russian Federation. It is not yet known whether any such designation has effect in other States of the former Soviet Union.

**METHOD FOR MAKING UNIFORMLY-SIZED PARTICLES
FROM INSOLUBLE COMPOUNDS**

5

BACKGROUND OF THE INVENTION

Particles of compounds having low solubility in a dispersing medium are commonly used in a wide variety of applications, including pharmaceuticals, ceramics, paints, inks, dyes, lubricants, pesticides, 10 insecticides, fungicides, fertilizers, chromatography columns, cosmetics, lotions, ointments, and detergents. Aqueous dispersions of particles are used in many cases to avoid hazards such as flammability and toxicity associated with organic solvents. Such dispersions 15 typically have a broad range of particle size.

In many cases product performance is improved by controlling the particle size distribution. In general, smaller particles of a compound provide a more uniform 20 dispersion and will dissolve faster than larger particles of the same compounds. Control of particle size is, therefore, important in controlling the rate of solubilization.

25 Many drugs have been formulated as particles for sustained-release following oral, aerosol, subcutaneous, intramuscular, or other routes of administration. Particle size is one important factor affecting the

-2-

release rate of these drugs. Those skilled in the art can discern other examples for using particle size to control product performance for the substances listed above.

5

Drugs that are insoluble in water can have significant benefits when formulated as a stable suspension of particles of less than three microns diameter. In this particulate form, the drug can be injected

- 10 intravenously, circulate in blood, and be preferentially accumulated in, for example, the reticuloendothelial system, where it can facilitate normal reticuloendothelial functions such as detoxification. Alternatively, the drug can reside in the
- 15 reticuloendothelial cells where it is stored until solubilized or metabolized into an active form which circulates in blood to other tissues for efficacy. This "slow" release of active drug can provide more constant drug concentrations in plasma over a period of hours,
- 20 days, weeks, or months, resulting in improved therapeutic efficacy. Biodegradable particles which are radiopaque or labelled with a radioisotope are useful for diagnostic imaging of organs, such as liver and spleen, with high concentrations of fixed
- 25 reticuloendothelial function.

Many advantages have already been recognized for insoluble particulate radiopaque contrast media, for example, as explained in "Improvement in Radiographic Contrast Media Through the Development of Colloidal or Particulate Media: an Analysis", by Harry W. Fischer, Journal of Theoretical Biology, 67: 653-670 (1977). More recent papers on this subject include Violante, M. R., Fischer, H. W., and Mahoney, J.A., "Particulate Contrast Media," Invest. Radiol., 15: S329 November-December 1980; and Violante, M. R., Dean, P. B.,

-3-

Fischer, H. W., and Mahoney, J. A., "Particulate Contrast Media for Computer Tomographic Scanning of the Liver", Invest. Radiol., 15: 171 November-December 1980.

5 There are enormous medical implications for the intravenous administration of drugs formulated as suspensions of particles of three microns diameter, or less, which can be accumulated by phagocytic cells and slowly solubilized for sustained release into plasma for
10 circulation to other organs and tissues. Obvious drug classes appropriate for formulation as particulate suspensions include: antineoplastics, antimicrobials, antivirals, anticoagulants, antihypertensives, antihistamines, antimalarials, male and female
15 contraceptives, antiepileptics, depressants and antidepressants, adrenocortical steroids, hormones and hormone antagonists, cardiac glycosides, immunosuppressants, beta-blockers, water-insoluble vitamins, sympathomimetics, hypoglycemic agents,
20 hyperglycemic agents, analgesics, tranquilizers, mood altering drugs, and others. The treatment of deficiency diseases, alcohol abuse, drug abuse, and many others could be improved with intravenous administration of particulate suspensions of the appropriate drug. Other
25 medical applications for particulate drug suspensions will be apparent to those skilled in the art.

Accurate control of particle size is essential for safe and efficacious use of these formulations. Particles
30 must be less than three microns in diameter to safely pass through capillaries without causing emboli. This is critical for intravenous administration since the particles must pass through lung capillaries before reaching the fixed reticuloendothelial cells of liver
35 and spleen. Restriction to particle diameters of 0.01-0.1 micron could result in selective accumulation of

-4-

these particles in certain tissues, eg., neoplastic tissue, where capillaries are somewhat more porous than capillaries of normal tissues. Suspensions of particles with diameters greater than 10 microns could be useful
5 for selective intra-arterial administration to purposely embolize vessels feeding abnormal tissue such as a neoplasm. Accurate and precise control of particle diameters is essential for efficacy while minimizing or avoiding adverse effects in each of these applications.

10

Conventional methods of making insoluble compounds produce particles of many different sizes, many of which are unsuitable for the purpose at hand. Mechanically sorting or separating a desired particle size from a mix
15 of sizes is difficult and unsatisfactory. Centrifuging and filtration do not produce high yields of particles that are all precisely the same desired size.

Investigations of water-insoluble radiopaque contrast
20 materials required uniform particles in specific sizes that were very difficult to obtain by conventional methods. Precipitation as a way of directly forming particles of a predetermined size was then investigated. Partial success was achieved with one material and one
25 method as reported in "Particulate Contrast Media", Investigative Radiology, 15: S329 November-December 1980; but this method would not work with other materials and would not allow accurate variation and control of the particle size produced.

30

Further investigation led to the invention of this application, which is effective with any compound having a solubility in a given liquid of preferably less than one part per ten thousand to obtain a predetermined
35 particle size of the compound in a dispersion.

-5-

SUMMARY OF THE INVENTION

The invention involves a method of making uniformly sized particles of a solid compound by, first, preparing 5 a solution of the solid compound in a suitable solvent for the compound, second, infusing a precipitating liquid into the solution at a temperature between about -50°C and about 100°C and at an infusion rate of from about 0.01 ml per minute to about 3000 ml per minute per 10 unit volume of 50 ml, the solid compound having essentially little solubility in the precipitating liquid and the solvent being miscible in the precipitating liquid, so as to produce a suspension of precipitated solid compound in the form of substantially 15 non-aggregated particles with a substantially uniform mean particle diameter selected from the range of up to about 10 microns, such that the particle size is directly related to the solution temperature and inversely related to infusion rate, and then separating 20 the particles from the solvent and washing in a suitable washing liquid.

In preferred embodiments of the invention, additional precipitating liquid is added to the suspension before 25 the particles are separated from the solvent. Separation can be accomplished, for example, by centrifugation, membrane filtration, reverse osmosis, or other methods.

30 The mean particle diameter of the particles can be up to about 10 microns, preferably in a range of 0.01 microns to about 5 microns.

Particles made according to this invention will 35 typically have a particle size distribution with a maximum relative standard deviation of 30%, for example

-6-

95% of the particle having a mean size of 1.0 micron will be within the size range of 0.5 to 1.5 microns.

The present invention is useful for compounds which 5 preferably have essentially little solubility in a precipitating liquid, i.e. a solubility of less than about one part per ten thousand in the precipitating liquid. Generally, any compound that meets the other requirements of the invention is suitable, including 10 many drugs. The compound may be organic or inorganic.

The solvent may be organic or inorganic, as long as the solubility of the compound in the solvent is greater than about 10 mg/ml. Also, the solvent must be miscible 15 with the precipitating liquid.

The washing liquid can be the same as or different than the precipitating liquid. In certain instances it may be advantageous for the compound to have a lower 20 solubility in the washing liquid than in the precipitating liquid in order to maximize yield.

When the solid compound has essentially little aqueous solubility, the precipitating liquid can be water, a 25 solution of a mineral salt, a surfactant solution, or an organic solvent in which the compound is poorly soluble. Suitable aqueous surfactant solutions include 5% polyvinylpyrrolidone C-30, 0.1% polyvinylpyrrolidone C-15, 0.1% human serum albumin, 0.1% Pluronic F-68 30 (poloxamer 188), and 0.33% gelatin, alone or combined with 0.6% hetastarch, 0.02% propylene glycol, or 2% sucrose. The organic solvent can be dimethyl sulfoxide, dimethyl formamide, N,N'-dimethyl acetamide, phenol, isopropanol, or other solvents.

35

In one embodiment of the invention, the solid compound

-7-

has poor aqueous solubility, i.e. an aqueous solubility from about one part per ten thousand to about one part per one hundred. This embodiment is particularly suitable for situations where a compound which might 5 normally be considered water-insoluble encounters a significant yield loss when precipitated in an aqueous solution. In order to improve yield, a precipitating and washing liquid may be chosen in which the compound is even less soluble than water. In this embodiment, 10 the solvents which may be used include the organic solvents previously identified, among others. However, the precipitating liquid is at least substantially non-aqueous. Suitable non-aqueous solutions include alcohols such as ethanol, and alcoholic surfactant 15 solutions such as 1% (w/v) polyvinylpyrrolidone in ethanol, other lower aliphatic alcohols, acids, amides, aldehydes, ketones, and glycols.

In one embodiment, the method includes the additional 20 step of diluting the solution in which the compound is dissolved with a non-solvent, i.e. a liquid in which the compound is poorly soluble but does not cause the compound to precipitate, such that the ratio of non-solvent to solvent is between about 100:1 and about 25 1:100, after preparing the solution and before the infusion step, so that the particle size is directly related to the ratio of non-solvent to solvent.

In one preferred embodiment, the solid compound is 30 iodipamide ethyl ester, an ethyl ester of a triiodobenzoic acid derivative, and is dissolved in dimethyl sulfoxide and diluted with ethanol. The compound is thereafter precipitated with an aqueous surfactant solution. If the ratio of ethanol to 35 dimethyl sulfoxide is greater than about two, the mean particle diameter is greater than about one micron, and

-8-

if the ratio of ethanol to dimethyl sulfoxide is less than about two, the mean particle diameter is less than about one micron.

- 5 In another preferred embodiment, the solid compound is mitindomide, an anticancer drug having the molecular formula $C_{14}H_{12}N_2O_4$ and a molecular weight of 272.3. The mitindomide is dissolved in dimethyl sulfoxide and the precipitating liquid used is 1% (w/v) 10 polyvinylpyrrolidone in 99% ethanol.

In yet another preferred embodiment, the solid compound is aluminum chloride hexahydrate. It is dissolved in ethanol (99%), and thereafter diluted with acetone. The 15 compound is then precipitated with an aqueous surfactant solution.

BRIEF DESCRIPTION OF THE DRAWINGS

- 20 Figure 1 is a graph of free energy of the various phases of the compounds used in the invention.

Figure 2 is a graph of the relationship between size distribution of particles and time interval between 25 onset and completion of precipitation.

- 30 Figure 3 is a graph of infusion rate (ml/min.) (of aqueous precipitating liquid) as a function of the product of stir rate (rpm) and total volume (liters) of the organic solution at a constant temperature; the relationship: aqueous infusion rate (ml/min.) = 23 + 0.14 [stir rate (rpm) x volume organic solution (l)] defines the parameters for production of iodipamide ethyl ester particles of one micron diameter at a 35 constant temperature (4°C) and in dimethyl sulfoxide/ethanol;

-9-

Figure 4 is a graph showing iodipamide ethyl ester particle size as a function of temperature at a constant ratio of infusion rate of aqueous precipitating liquid to [stir rate (rpm) x volume of organic solution];

5

Figure 5 is a graph demonstrating the effect on particle size of varying the infusion rate of aqueous precipitating liquid at constant temperature and stirring rate of an iodipamide ethyl ester solution; and

10

Figure 6 is a schematic diagram of preferred steps in the inventive method.

DETAILED DESCRIPTION OF THE INVENTION

15

This invention concerns the preparation of uniform particles of a predetermined size. One aspect of the invention concerns the preparation of uniform particles of a predetermined size in a vehicle in which the

20 concentration of the compound in the vehicle is greater than the solubility of the compound in that vehicle.

The particles are formed by a carefully controlled precipitation of the compound into a suitable precipitating liquid from a solvent in which the

25 compound is soluble.

The physical chemical principles thought to be involved in this invention are demonstrated in Figures 1 and 2.

Figure 1 shows that the free energy of the system is

30 higher when the compound is dissolved in the organic solvent than when the compound exists in the particulate or crystalline state. During precipitation the compound will naturally convert to the crystalline form--the lowest free energy state--unless it is trapped in the

35 metastable particulate form, a condition where its free energy is intermediate between the solution and the

-10-

crystalline phases. When properly practiced, this invention enables the trapping of a compound in the metastable particle state, precluding transformation to the crystalline state.

5

The size distribution of particles formed during precipitation can be correlated with the time interval between onset and completion of precipitation. As shown in Figure 2, a very short time interval results in the 10 production of uniformly sized particles (A), while a very long time interval results in a broad particle size distribution (B). Intermediate conditions produce intermediate particle size distributions.

15 An important parameter for utilization of this invention is the solubility of the compound in the precipitating liquid. Thus, compounds having essentially little aqueous solubility, i.e. compounds which have an aqueous solubility of less than one part in ten thousand, may be 20 precipitated in an aqueous solution in order to obtain an excellent yield. Compounds which are more water-soluble can also use an aqueous precipitating liquid. However, the higher the solubility of the compound, the greater the probability that some of the compound will 25 dissolve in the aqueous phase and transform to the more stable crystalline state. Also, redissolution in the aqueous phase can lead to a broadening of the particle size distribution. For these reasons, it is preferred that an aqueous precipitating liquid be used for 30 compounds having a water-solubility of less than one part in ten thousand.

It has been found that it is possible to prepare suspensions of compounds which are poorly soluble in 35 aqueous solutions, i.e., have a solubility from about one part per ten thousand to about one part per one

-11-

hundred which provide excellent yields by using an acceptable precipitating liquid in which the compounds have even less solubility than water. The difference in the solubility of the compound in water as compared to 5 the precipitating liquid need not be large in order to be significant in terms of yield.

In order to make particles of a uniform and predetermined size, a solution of the solid compound in 10 a suitable solvent is prepared. The solution may be diluted with a non-solvent that does not cause the drug or other compound to precipitate. A precipitating liquid is also prepared, preferably with a surfactant, in sufficient quantity to both precipitate the drug or 15 other compound and stabilize the resulting suspension of particles of the compound against aggregation. The precipitating liquid may be used alone when compounds which do not aggregate are used. The precipitating liquid is infused into the solution in which the 20 compound is dissolved under carefully controlled conditions, including: the rate of stirring of the organic solution, the rate of infusion of the aqueous solution, the volume of the organic solution and the temperature of the solutions and the suspension. The 25 precipitating liquid may be infused, for example, through a needle of standard gauge.

In investigations of varying parameters to adjust for particle size, three usable relationships were 30 discovered: (1) diluting the solution with more of the non-solvent produces larger particles, and diluting with less of the non-solvent produces smaller particles; (2) higher temperatures of the solution during precipitation produce larger particles, and lower temperatures of the 35 solution during precipitation produce smaller particles; and (3) at a given stirring rate of the organic

-12-

solution, faster infusion rates of precipitating liquid produce smaller particles while slower infusion rates produce larger particles.

5 When the precipitation is complete, the uniformly sized particles are washed to remove the solvent, i.e. by centrifugation, filtration, etc. In most cases, the particles should be separated from the solvent quickly to prevent transformation to a crystalline form.

10

Aqueous precipitating liquids are useful for many compounds, including but not limited to organic compounds such as iodipamide ethyl ester, iothalamate ethyl ester, iosefamate ethyl ester, 2,2', 4,4' -

15 tetrahydroxybenzophenone, RS nitrocellulose, progesterone, beta-2,4,6-triiodo-3-dimethyl formamidinophenyl propionic acid ethyl ester, isopropylpyrrolizine derivative (NSC-278214), N-(trifluoroacetyl) Adriamycin 14 valerate, 1,2
20 diaminocyclohexane malinate platinum (II), norethisterone, acetyl salicylic acid, warfarin, heparin-tridodecyl methyl ammonium chloride complex, sulfamethoxazole, cephalexin, prednisolone acetate, diazepam, clonazepam, methidone, naloxone, disulfiram, 25 mercaptopurine, digitoxin, primaguine, mefloquine, atropine, scopolamine, thiazide, furosemide, propanalol, methyl methacrylate, poly methyl methacrylate, 5-fluorodeoxyuridine, cytosine arabinoside, acyclovir, and levonorgestrel; and inorganic compounds such as aluminum
30 chloride hexahydrate, the oxides of iron, copper, manganese, tin.

Compounds which are better suited for precipitation using a non-aqueous precipitating liquid include organic
35 compounds such as mitindomide, hydrolytically unstable compounds such as isopropylpyrrolizine (IPP, or carbamic

-13-

acid, (1-methylethyl)-, (5-(3,4-dichlorophenol)-2,3-dihydro-1, H-pyrrolizine-6,7-diyl) bis(methylene ester); and inorganic compounds such as iron citrate, iron iodate, calcium pyrophosphate, calcium salicylate, 5 platinum dichloride and sodium pyrophosphate.

The first step is to prepare a solution of the compound of interest in a suitable solvent for that compound. This can occur as the compound is synthesized as a 10 dissolved solid, or it can be done by simply dissolving the compound in the solvent of choice.

The solvent is chosen to suit the compound. For example, dimethylformamide (DMF) is a solvent for 15 iothalamate ethyl ester (IEE) and iosefamate ethyl ester (IFE), and dimethylsulfoxide (DMSO) is a solvent for iodipamide ethyl ester (IDE) and IEE. DMSO is also a suitable solvent for compounds such as mitindomide. Another suitable solvent for many compounds, and 20 especially IPP, is tetrahydrofuran (THF).

The solution is then optionally diluted with a non-solvent that does not cause the compound to precipitate. The non-solvent causes greater dispersion of the 25 dissolved molecules of the compound in the liquid phase. Greater dilution of the solution with non-solvent produces larger particles, and less dilution of the solution with non-solvent produces smaller particles.

30 The non-solvent should not precipitate the compound when it is added to the solution. Lower aliphatic alcohols, such as ethanol, are effective non-solvents for solutions of IDE and IEE in DMSO. For the ethyl esters of triiodobenzoic acid, proportions of non-solvent to 35 solvent at a ratio of 2 or more can produce 1 to 3 micron sized particles (depending on other parameters);

-14-

and ratios of less than 2 can produce sub-micron particles, at least as applied to DMSO solutions diluted with ethanol.

- 5 To precipitate the compound from the solution in a desired particle size, a solution of a surfactant is prepared in sufficient quantity to effect complete precipitation of the compound and to stabilize the resulting suspension of particles of the compound
- 10 against aggregation. The surfactant provides the stabilization against aggregation, while a suitable precipitating agent causes the precipitation of the compound. Presence of extra surfactant solution is advisable to ensure stabilization so that precipitated
- 15 particles suspended in liquid do not aggregate, forming agglomerates of an improperly large size. While surfactants are used in most cases, some compounds appear to form stable, substantially non-aggregated particles without the use of surfactants. Examples of
- 20 such non-aggregating compounds are certain heparin complexes.

It is thought that particles with relatively high surface charge are less likely to require surfactant in the precipitating solution. The surface charge of a particle is sometimes referred to as its zeta potential, a measurement of charge which falls off with distance. There may be a threshold zeta potential above which no surfactant is needed, but below which, surfactant is

25 needed to keep the precipitating particles from aggregating. The zeta potential is directly correlated with the polarity or net charge of a compound. Thus, the need for surfactant in the precipitating solution may be predicted from the extent of the charge or

30 polarity of the compound employed in the method of the invention. For example, heparin complexes are highly

-15-

charged, and form stable non-aggregated particles when precipitated with water.

Generally, such a theory notwithstanding, empirical

5 methods will suffice; that is, a precipitation may first be performed with water, and if aggregation occurs, then a precipitation in the presence of surfactant is indicated. Surfactants are chosen for their compatibility with the compound and their ability to

10 stabilize a suspension of compound particles. For work with IEE and IDE drugs, a solution of 5% polyvinylpyrrolidone (C-30), 0.1% polyvinylpyrrolidone (C-15), or 0.1% human serum albumin is preferred. Also 0.1% Pluronic F-68, [Poloxamer 188, a poly(oxyethylene-

15 co-oxypropylene) polymer], a 0.33% gelatin, 0.33% gelatin plus 0.6% Hetastarch, 0.33% gelatin plus 0.002% propylene glycol, and 0.33% gelatin plus 2% sucrose, or other surfactants known to one skilled in the art can be used.

20 To precipitate particles of the compound in the desired sizes, the precipitating liquid and the solution are combined under controlled conditions of temperature, ratio of infusion rate to stirring rate, and the

25 proportion of non-solvent to solvent in the dispersed solution.

30 Preferably, the solution being infused with precipitating liquid is agitated. This can be accomplished by stirring, shaking, by the infusion itself and by other techniques known to those skilled in the art. This effect can also be achieved by combining a stream of precipitating liquid with a stream of the solution.

35 The precipitation of the compound occurs exothermically,

-16-

heating the solution and the resulting suspension. The temperature of the solution and resulting suspension is controlled to achieve the particle size of precipitate that is desired. Higher solution temperatures during 5 precipitation produce larger particles, and lower solution temperatures during precipitation produce smaller particles. Since many compounds are less soluble at lower temperatures, it is generally preferred to conduct the infusion of precipitating liquid at a low 10 temperature in order to maximize yield. The lower limit of the temperature at which precipitation can be conducted is, of course dependent upon the freezing point of the solvent, precipitating liquid, as well as economic concerns.

15

Also, faster infusion rates at constant stirring rate of organic solution produce smaller particles, and slower infusion rates produce larger particles.

20 FIGS. 3-5 show the effects on particle size of varying parameters during precipitation of IDE from a DMSO solution diluted with 1 part solution to 2 parts ethanol using an aqueous solution of 5% polyvinylpyrrolidone at different infusion rates and temperatures.

25

FIG. 3 shows that as the volume and stirring rate of the organic compound iodipamide ethyl ester and dimethyl sulfoxide/ethanol solution are increased, the infusion rate of aqueous surfactant solution must be increased 30 proportionally as defined by: infusion rate (ml/min.) = $23 + 0.14 [\text{volume (liters)} \times \text{stir rate (r.p.m.)}]$ to produce particles of 1 micron diameter at 4°C.

35 FIG. 4 shows that at a constant ratio of infusion rate to [stir rate x volume], increased precipitation temperature produces larger particles.

-17-

FIG. 5 plots 3 points from the 20°C temperature line of FIG. 3 for rate of infusion of the precipitating liquid into the organic solution to approximate the curve by which larger particles are formed from slower injection 5 rates, showing that at a constant ratio of temperature to [stir rate x volume], particle size is inversely related to the rate of infusion of the precipitating liquid.

10 When FIGS. 3-5 are considered together, they show clearly that higher temperatures and slower mixing rates produce larger particles, and lower temperatures and faster mixing rates produce smaller particles. Another parameter that can be varied to affect particle size is 15 the amount of dilution of the solution before precipitation occurs.

When the precipitation is complete, extra surfactant solution can be added to further stabilize the suspended 20 particles against agglomeration. The extra solution can be added at a rapid rate, since essentially all the compound is now precipitated in uniformly sized particles. The precipitated particles are promptly separated from the solvent to prevent redissolving and 25 reprecipitation of particles at undesirable sizes. Centrifuging is a preferred way to perform the separation. Other methods, including membrane filtration, reverse osmosis, and others known to persons skilled in the art may also be used to remove undesired 30 substances. Promptly after separating the particles, the particles are washed or rinsed with normal saline solution to remove solvent and excess surfactant. Where an aqueous precipitating liquid is used, normal saline solution may be used for this purpose.

35

The particles prepared according to the method outlined

SUBSTITUTE SHEET

-18-

above may be resuspended in an appropriate suspension vehicle which may be aqueous or non-aqueous solution, as the situation requires. For example where the particles formed comprise a pharmaceutical compound for parenteral 5 administration, the particles are ultimately resuspended in an aqueous solution such as sterile water. In other instances, the particles may be suspended in a carrying agent such as an ointment, gel, or the like. Preferably, the compound has the same range of 10 solubility in the suspension vehicle as in the precipitating liquid.

The method of the invention is illustrated by the following examples which, however, do not limit the 15 invention as described above and set forth in the claims.

Examples 1 to 19 are presented in Table I. The solid organic compound was dissolved in the organic solvent 20 and then diluted (except where indicated) by the non-solvent. The aqueous precipitating liquid was then infused through a needle at the given rate into the solution, at the given temperature and while stirring at the given stirring rate. The size of the particles 25 obtained is shown for each example.

-19-

Table Ia

		Example 1	Example 2
5	1.	solid organic compound	10 mg 2,2',4,4',-tetra-hydroxybenzophenone
10			1.4 mg RS nitro-cellulose compound (1/4 sec)
15	2.	organic solvent	0.2 ml dimethyl sulfoxide
20	3.	non-solvent	0.2 ml ethanol (99%)
25	4.	aqueous precipitating liquid	5 ml human serum albumin (0.1%)
30	5.	infusion rate (ml/min.) of precipitating liquid	2.5 2
35	6.	stir rate (rev./min) of solution	200 400
40	7.	temperature of solution	20°C 20°C
45	8.	particle diameter	0.5 micron 0.5 micron

Table Ib

		Example 3	Example 4
40	1.	solid organic progesterone compound	7 mg RS nitrocellulose (1/4 sec.) 10 mg
45	2.	organic solvent	0.4 ml dimethyl sulfoxide 0.2 ml dimethyl sulfoxide
50	3.	non-solvent	0.01 ml isopropanol 0.2 ml ethanol (99%)

-20-

4.	aqueous precipitating liquid	5 ml human serum albumin (0.1%)	5 ml human serum albumin (0.1%)
5	5. infusion rate (ml/min.) of precipitating liquid	2.5	2.5 (through an 18 gauge needle)
10	6. stir rate (rev./min) of solution	200	200
15	7. temperature of solution	20°C	20°C
	8. particle diameter	0.5 micron	1 micron

Table Ic

	Example 5	Example 6
20	1. solid organic compound	5240 mg iosefamate ethyl ester
25	2. organic solvent	60 ml dimethyl sulfoxide
30	3. non-solvent	20 ml ethanol (99%)
35	4. aqueous precipitating liquid	400 ml polyvinyl pyrrolidone C-15 (5%)
40	5. infusion rate (ml/min.) of precipitating liquid	3 300
45	6. stir rate (rev./min) of solution	200 300
	7. temperature of solution	20°C 0-2°C initial 40°C final
	8. particle diameter	1.0 micron 1.0 micron diameter

-21-

Table Ia

		Example 7	Example 8
5	1. solid organic compound	100 mg beta-2,3,6 triod-3-dimethyl formamidino-phenyl propionic acid ethyl ester	100 mg beta-2,3,6 triod-3-dimethyl formamidino-phenyl propionic acid ethyl ester
10	2. organic solvent	2.0 ml dimethyl sulfoxide	2.0 ml dimethyl sulfoxide
15	3. non-solvent	2.5 ml ethanol (99%)	2.5 ml ethanol (99%)
20	4. aqueous precipitating liquid	25 ml Poloxamer 188 a poly (oxyethylene-co-oxypropylene) polymer (Pluronic F-68)(0.1%)	25 ml human serum albumin (0.1%)
25	5. infusion rate (ml/min.) of precipitating liquid	750	750
30	6. stir rate (rev./min) of solution	650	650
35	7. temperature of solution	10°C	10°C
	8. particle diameter	0.1 micron	0.1 micron

Table Ie

		Example 9	Example 10
40	1. solid organic compound	100 mg beta 2,4,6-triiod-iodipamide 3-dimethyl formamidino phenyl propionic acid ethyl ester	120 mg ethyl ester
45	2. organic solvent	2.0 ml dimethyl sulfoxide	2.0 ml dimethyl sulfoxide
50	3. non-solvent	2.5 ml ethanol (99%)	2.5 ml ethanol (99%)

-22-

4.	aqueous precipitating liquid	25 ml polyvinyl pyrrolidone C-15 (0.1%)	5 ml polyvinyl pyrrolidone C-15 (0.1%)
5	5.	infusion rate (ml/min.) of precipitating liquid	750 300
10	6.	stir rate (rev./min) of solution	650 80
15	7.	temperature of solution	10°C 4°C
	8.	particle diameter	0.1 micron 0.1 micron

20 Table If

		Example 11	Example 12
25	1.	solid organic compound	1200 mg iodipamide ethyl ester 120 mg iodipamide ethyl ester
30	2.	organic solvent	20 ml dimethyl sulfoxide 2.0 ml dimethyl sulfoxide
35	3.	non-solvent	25 ml ethanol (99%) 2.5 ml ethanol (99%)
40	4.	aqueous precipitating liquid	50 ml polyvinyl pyrrolidone C-15 (0.1%) 5.0 ml polyvinyl pyrrolidone C-15 (0.1%)
45	5.	infusion rate (ml/min.) of precipitating liquid	19 2
	6.	stir rate (rev./min) of solution	190 200
	7.	temperature of solution	10°C 10°C
	8.	particle diameter	1.5 micron 1.0 micron

-23-

Table Ia

		Example 13	Example 14
5	1. solid organic compound	120 mg iodipamide ethyl ester	10 mg isopropyl pyrrolizine derivative (NSC-278214)
10	2. organic solvent	2.0 ml dimethyl sulfoxide	0.4 ml dimethyl sulfoxide
15	3. non-solvent	2.5 ml ethanol (99%)	--
20	4. aqueous precipitating liquid	25 ml poly(oxyethylene co-oxypropylene) polymer, Poloxamer 188 (Pluronic F-65) (0.1%)	5 ml human serum albumin (0.1%)
25	5. infusion rate (ml/min.) of precipitating liquid	750	20
30	6. stir rate (rev./min) of solution	700	300
35	7. temperature of solution	0°C	17°C
	8. particle diameter	0.1 micron	0.5 micron

Table Ib

		Example 15	Example 16
40	1. solid organic compound	10 mg isopropyl pyrrolizine derivative (NSC-278214)	10 mg isopropyl pyrrolizine derivative (NSC-278214)
45	2. organic solvent	0.4 ml N,N'-dimethyl acetamide	0.4 ml dimethyl sulfoxide
50	3. non-solvent	--	0.2 ml ethanol (99%)

-24-

4.	aqueous precipitating liquid	20 ml human serum albumin (0.1%)	20 ml human serum albumin (0.1%)
5	5. infusion rate (ml/min.) of precipitating liquid	38	100
10	6. stir rate (rev./min) of solution	50	200
15	7. temperature of solution	0°C	0°C
	8. particle diameter	0.5 micron	0.1 micron

Table II

		Example 17	Example 18
20	1. solid organic compound	1.5 mg. 1,2 diamino-cyclohexane malinate platinum (II)	10 mg N-(trifluoroacetyl) adriomycin 14 valerate
25	2. organic solvent	0.05 ml phenol	0.2 ml dimethyl sulfoxide
30	3. non-solvent	0.45 ml m-amino-phenol and 0.25 ml ethanol (99%)	0.2 ml ethanol (99%)
35	4. aqueous precipitating liquid	5 ml human serum albumin (0.1%)	5 ml human serum albumin (0.1%)
40	5. infusion rate (ml/min.) of precipitating liquid	5	2.5
45	6. stir rate (rev./min) of solution	200	200
50	7. temperature of solution	20°C	20°C
	8. particle diameter	0.1 micron	1.0 micron

-25-

Table II

	Example 19	Example 20
5	1. solid organic compound 200 mg heparin-benzal-konium chloride complex	10 mg organic compound* (see list)
10	2. organic solvent 10 ml isopropanol	0.2 ml dimethyl sulfoxide
	3. non-solvent --	0.2 ml ethanol (99%)
15	4. aqueous precipitating liquid 200 ml water	5 ml human serum albumin (0.1%)
20	5. infusion rate (ml/min.) of precipitating liquid 3.7	2.5
25	6. stir rate (rev./min) of solution 300	250
	7. temperature of solution 20°C	20°C
30	8. particle diameter 0.5 micron	1.0 micron

*norethisterone,
acetyl salicylic acid,
35 wafarin,
heparin-tridodecyl methyl ammonium chloride complex,
sulfamethoxazole,
cephalexin,
prednisolone acetate,

40 diazepam,
clonazepam,
methidone,
naloxone,
disulfiram,
45 mercaptopurine,
digitoxin,
primaquine,
mefloquine,
atropine,
50 scopolamine,
thiazide,
furosemide,
propanolol,
methyl methacrylate,
55 poly methyl methacrylate,

-26-

5-fluorodeoxyuridine,
cytosine arabinoside,
acyclovir,
levonorgestrel

5 Examples 1 to 19 show how the process can be used to produce aqueous dispersions of a wide variety of compounds that have low aqueous solubility and for which particle size can be controlled with substantial

10 10 precision and predictability. Conditions would be varied from compound to compound according to the invention in order to optimize results. This may in some cases include chemical modification of the compound to achieve the desired solubility.

15 Because of the range of examples presented above, it is reasonable to one skilled in the art, that numerous other compounds would be expected to behave in similar fashion.

20 Example 20 is also presented in Table I. This example should be performed in the same manner as examples 1 to 19, and would make particles of the listed compounds within the scope of the invention.

25 Examples 21 to 28 are presented in Table II. In each example, the given quantity of iodipamide ethyl ester was dissolved in the given volume of dimethyl sulfoxide, then diluted with the given volume of ethanol. The

30 30 aqueous precipitating liquid was prepared from polyvinylpyrrolidone then infused at the given infusion rate through a needle with the given gauge into the solution while the solution was stirred at the given stir rate. The precipitation was carried out in the

35 35 given vessel at the given temperature. After precipitation, the given amount of saline was added to further stabilize the dispersion. In each example, the mean particle diameter was about 1.0 micron and

-27-

substantially uniform.

TABLE IIa

Parameters for Iodipamide Ethyl Ester Particle Precipitation

5

		Example 21	Example 22	Example 23
10	Material	0.5 gm	1 gm	2 gm
	iodipamide ethyl ester (60 mg/ml)	10 ml	20 ml	40 ml
15	ethanol (99%)	12.5 ml	25 ml	50 ml
	polyvinyl pyrrolidone	25 ml	50 ml	100 ml
20	0.9% saline	15 ml	30 ml	60 ml
	stir rate	125 rpm	190 rpm	300 rpm
	temperature	4°C	4°C	4°C
25	infusion rate	11 ml/min	19 ml/min	30 ml/min
	infusion needle size	19 g	19 g	19 g
30	S.B. length	1.5"	1.5"	1.5"
	vessel diam.	2.38"	2.38"	2.38"
35	vessel	250 ml	250 ml	250 ml
		polypropylene bottle	polypropylene bottle	polypropylene breaker

TABLE IIb

40

Parameters for Iodipamide Ethyl Ester Particle Precipitation

		Example 24	Example 25	Example 26
45	Material	3.5 gm	5 gm	10 gm
	iodipamide ethyl ester (60 mg/ml)	70 ml	100 ml	200 ml
50	ethanol (99%)	87.5 ml	125 ml	250 ml
	polyvinyl	175 ml	250 ml	500 ml

-28-

	pyrrolidone		
	0.9% saline	105 ml	150 ml
5	stir rate	330 rpm	200 rpm
	temperature	--	--
10	infusion rate	45 ml/min	60 ml/min
	infusion needle size	19 g	18 g
15	S.B. length	1.88"	2.75"
	vessel diam.	3.38"	5.0"
20	vessel	1,000 ml	2,000 ml
		glass beaker	glass beaker

TABLE IIc

25 Parameters for Iodipamide Ethyl Ester Particle Precipitation

	Example 27	Example 28
30	Material	20 gm
		40 gm
	iodipamide ethyl ester (60 mg/ml)	400 ml
35	ethanol (99%)	800 ml
		500 ml
40	polyvinyl pyrrolidone	1,000 ml
		2,000 ml
	0.9% saline	600 ml
		1,200 ml
	stir rate	175 rpm
45	temperature	210 rpm
	--	--
	infusion rate	120 ml/min
		175 ml/min
50	infusion needle size	16 g
		16 g
	S.B. length	3.25"
		3.25"
55	vessel diam.	8.6"
		8.6"

-29-

vessel	9 L	9 L
	Bellco vessel	Bellco vessel

5

EXAMPLE 29

**PREPARATION OF IODIPAMIDE ETHYL ESTER
PARTICLES FOR ADMINISTRATION TO A PATIENT.**

10 Particles of iodipamide ethyl ester (IDE) with a size of about 1 micron may be prepared for administration to a patient. IDE is the water-insoluble ethyl ester of iodipamide, a water-soluble radiopaque compound used clinically for radiographic examination of the
15 gallbladder. The synthesis of iodipamide ethyl ester is known in the art (for example, esterification by alcohol and acid or by a Schotten-Bauman reaction).

IDE is only minimally soluble in water (10^{-5} M) and can
20 be precipitated easily from the dimethyl sulfoxide (DMSO)/ethanol solvent mixture. However, the simple addition of water to this solution results in IDE particles with extremely rough contours; these particles vary in size from less than one micron to greater than
25 300 microns in diameter. In light of the problems that rough contours could damage vascular endothelial cells and promote aggregation, and that large particles could create pulmonary emboli, the method of this invention provides a more refined procedure for controlling
30 particle size and shape.

Particle Precipitation Procedure. Physical methods for modifying and controlling particle size, such as ball milling, grinding or sonication result in preparations
35 with a very broad range of particle diameters. These methods are commonly used to eliminate large particles (greater than 4-5 microns) which could embolize in the pulmonary capillary bed, but generally some particles of

-30-

submicron size are also produced; these very small particles have been shown to be more toxic than 1-2 micron particles, possibly due to increased protein binding resulting from the much larger surface area 5 inherent with particles of smaller diameters, or possibly because of excessive uptake by bone marrow cells.

A chemical precipitation procedure for producing 10 particles of a given size was developed to avoid these problems. By adding an aqueous solution of polyvinylpyrrolidone, at controlled rates and temperatures, to IDE dissolved in a dimethyl sulfoxide/ethanol solvent, apparently spherical, 15 amorphous particles can be produced with an extremely narrow size distribution. For a particle preparation with a mean diameter of 1 micron, the total range of particle diameters is 0.4 to 2.0 microns with 90 per cent of the particles ranging in size between 0.5 and 20 1.5 microns, as determined by microscopy.

By carefully controlling precipitation parameters, particle preparations demonstrating different mean diameters, but with a similarly small range of 25 diameters, can be produced.

The IDE particles produced using this methodology are stable in whole blood with little apparent tendency toward aggregation. When suspended in whole blood, there 30 is essentially no tendency for one micron IDE particles to aggregate with themselves or with formed elements of blood. The IDE particles have smooth contours.

-31-

EXAMPLE 30
PREPARATION OF UNIFORMLY-SIZED
PARTICLES FROM INORGANIC COMPOUNDS

- 5 A 10% solution of aluminum chloride hexahydrate ($\text{AlCl}_3 \cdot 6\text{H}_2\text{O}$) is prepared by adding 1 gram of this compound to 10 ml of 99% ethanol. This mixture is heated to approximately 50°C until substantially all of the $\text{AlCl}_3 \cdot 6\text{H}_2\text{O}$ is dissolved. The solution was then
- 10 allowed to cool to room temperature. Subsequently, 5 ml of acetone is added to 2.5 ml of $\text{AlCl}_3 \cdot 6\text{H}_2\text{O}$ /ethanol solution in 25 ml beaker and cooled to 4°C. This solution is stirred rapidly using a magnetic stirrer.
- 15 Next, 5 ml of 0.5% aqueous polyvinylpyrrolidone (PVP) is infused into the solution at pH 5 at a rate of 114 ml/minute. Immediately after the infusion, the solution becomes hazy as particles of $\text{AlCl}_3 \cdot 6\text{H}_2\text{O}$ are formed. Examination under a microscope (400x) reveals the
- 20 presence of small spherical, monodispersed particles. The suspension is then centrifuged at 10,000 RPM for 15 minute and the pellet is resuspended in aqueous 0.1% PVP/0.9% NaCl solution. Laser light scattering analysis of this suspension reveals a mean particle diameter of
- 25 285 nm.

EXAMPLE 31

30 PREPARATION OF UNIFORMLY-SIZED
PARTICLES IN NON-AQUEOUS MEDIA

- Mitindomide, a pharmaceutical intended for parenteral administration, has a solubility in water of 70 ug/ml at room temperature. Although this normally is
- 35 considered to be water-insoluble, we encountered

-32-

significant yield loss when we precipitate and wash with an aqueous solution. The solubility of mitindomide in absolute ethanol is less than 4 ug/ml at room temperature. This solubility difference between water and ethanol, although small, is significant when one is concerned with manufacturing yields. Therefore, a procedure was developed for preparing mitindomide particles in ethanol. The final suspension is prepared in aqueous medium. However, most of the preparation involves non-aqueous solvents.

A mitindomide solution of 30 mg/ml in DMSO is prepared and filtered through an 0.2 micron nylon filter immediately prior to use. A 1% (w/v) polyvinylpyrrolidone (PVP) solution in 99% ethanol is prepared and filtered through an 0.2 micron filter immediately prior to use. The mitindomide particles are prepared by mixing the 1% PVP/ethanol solution at a rate of six (6) liters/minute with the mitindomide/DMSO solution at a rate of 250 ml/minute at a temperature of 0°C. After 90 minutes of recirculation at this temperature, laser light scattering analysis reveals a mean particle diameter of approximately 400 nm.

At this stage the suspension can be transferred to a 500 ml bottle for storage at -20°C until further processing is desired or one may proceed directly to the following procedures.

Before use, the suspension must be washed to remove DMSO. This is accomplished by centrifugation, filtration or by any other means known to one skilled in the art. The wash fluid can be water. However, to maximize yield, it is preferred to wash with the 99% ethanol.

-33-

After washing, the particles may be resuspended in ethanol and stored at -20°C.

When the suspension is to be prepared in final form, the 5 suspension is centrifuged and the separated mitindomide particles are resuspended in aqueous PVP solution. This suspension vehicle may contain other additives such as buffer, preservatives, or other excipients as may be deemed necessary. The resultant "concentrated" 10 suspension is then lyophilized to remove the ethanol and most of the water. The lyophil can be reconstituted by adding sterile water just prior to use.

The examples provided above are not meant to be 15 exclusive. Many other variations of the present invention would be obvious to those skilled in the art, and are contemplated to be within the scope of the appended claims.

-34-

WE CLAIM:

1. A method of making uniformly sized particles of a solid compound having an aqueous solubility from about one part per ten thousand to about one part per one hundred, comprising:
 - (a) preparing a solution of the solid compound in a suitable solvent for the compound;
 - (b) infusing a substantially non-aqueous precipitating liquid into the solution at a temperature between about -50°C and about 100°C and at an infusion rate of from about 0.01 ml per minute to about 3000 ml per minute per 50 ml unit volume of solution, the solid compound having essentially little solubility in the precipitating liquid and the solvent being miscible in the precipitating liquid, so as to produce a suspension of precipitated amorphous, non-crystalline solid compound in the form of substantially non-aggregated particles of a uniform size selected from a particle diameter range of up to about 10 microns, the particle size being directly related to the solution temperature during precipitation and inversely related to the infusion rate; and
 - (c) separating the particles from the solvent and washing in a suitable substantially non-aqueous washing liquid, said particles having essentially little solubility in said washing liquid.
2. The method according to claim 1, wherein additional

SUBSTITUTE SHEET

-35-

precipitating liquid is added to the suspension before the particles are separated.

3. The method according to claim 1, wherein the particles are separated by centrifugation, membrane filtration, or reverse osmosis.
4. The method according to claim 1, wherein the washing liquid is the same as the precipitating liquid.
5. The method according to claim 1, wherein the precipitating liquid is a surfactant solution.
6. The method according to claim 1, wherein the solution is prepared such that the concentration of the solid compound is near its solubility limit in the solvent.
7. The method according to claim 1, wherein the solvent is an organic solvent selected from the group consisting of dimethyl sulfoxide, dimethyl formamide, N,N'-dimethyl acetamide, phenol, isopropanol, ethanol and tetrahydrofuran.
8. The method according to claim 1, wherein the solid compound is mitindomide, the solvent is DMSO, and the precipitating liquid is a 1% (w/v) polyvinylpyrrolidone in 99% ethanol.
9. The method according to claim 1, wherein the precipitating liquid is infused into a stream of the solution.
10. The method according to claim 1, further comprising, before step (b), the step of measuring

-36-

the zeta potential of the solid compound and using the zeta potential to select a surfactant and to determine the amount of surfactant in the precipitating liquid which is required to prevent aggregation of particles.

11. The method according to claim 1, wherein the particles are resuspended in a suspending liquid which is pharmaceutically acceptable for injection into a patient.
12. A method of making uniformly sized particles of a solid compound having an organic solubility from less than about one part per ten thousand, comprising:
 - (a) preparing a solution of the solid compound in an aqueous solvent for the compound;
 - (b) infusing a substantially non-aqueous precipitating liquid into the solution at a temperature between about -50°C and about 100°C and at an infusion rate of from about 0.01 ml per minute to about 3000 ml per minute per 50 ml unit volume of solution, the solid compound having essentially little solubility in the precipitating liquid and the solvent being miscible in the precipitating liquid, so as to produce a suspension of precipitated amorphous, non-crystalline solid compound in the form of substantially non-aggregated particles of a uniform size selected from a particle of diameter range of up to about 10 microns, the particle size being directly related to the solution temperature during precipitation and inversely related to the infusion rate; and
 - (c) separating the particles from the solvent and washing in a substantially non-aqueous washing

-37-

liquid, said particles having essentially little solubility in said washing liquid.

13. The method according to claim 12, wherein the precipitating liquid comprises a surfactant solution.
14. A method of making uniformly sized particles of a solid inorganic compound, comprising:
 - (a) preparing a solution of the compound in a water-miscible solvent for the compounds;
 - (b) infusing an aqueous precipitating liquid into the solution at a temperature between about -50°C and about 100°C and at an infusion rate of from about 0.01 ml per minute to about 3000 ml per minute per 50 ml unit volume of solution, the solid compound having essentially little solubility in the precipitating liquid and the solvent being miscible in the precipitating liquid, so as to produce a suspension of precipitated amorphous, non-crystalline solid compound in the form of substantially non-aggregated particles of a uniform size selected from a particle diameter range of up to about 10 microns, the particle size being directly related to the solution temperature during precipitation and inversely related to the infusion rate; and
 - (c) separating the particles from the solvent and washing in aqueous washing liquid, said particles having essentially little solubility in said washing liquid.
15. The method according to claim 14, wherein the precipitating liquid comprises a surfactant solution.

-38-

16. The method according to claim 14, wherein the precipitating liquid is a surfactant solution selected from the group consisting of 5% polyvinylpyrrolidone in water, 0.1% polyvinylpyrrolidone in water, 0.1% human serum albumin in water, 0.1% of a poly (oxyethylene-co-oxypropylene) polymer with average molecular weight of 8350 formed by addition of propylene oxide to the two hydroxyl groups of a propylene glycol initiator, 0.33% gelatin in water, 0.33% gelatin and 0.6% hetastarch in water, 0.33% gelatin and 0.02% propylene glycol in water, and 0.33% gelatin and 2% sucrose in water.
17. The method according to claim 16, wherein the solid compound is aluminum chloride hexahydrate, the solvent is ethanol, and the precipitating liquid is a 0.5% aqueous polyvinylpyrrolidone solution.

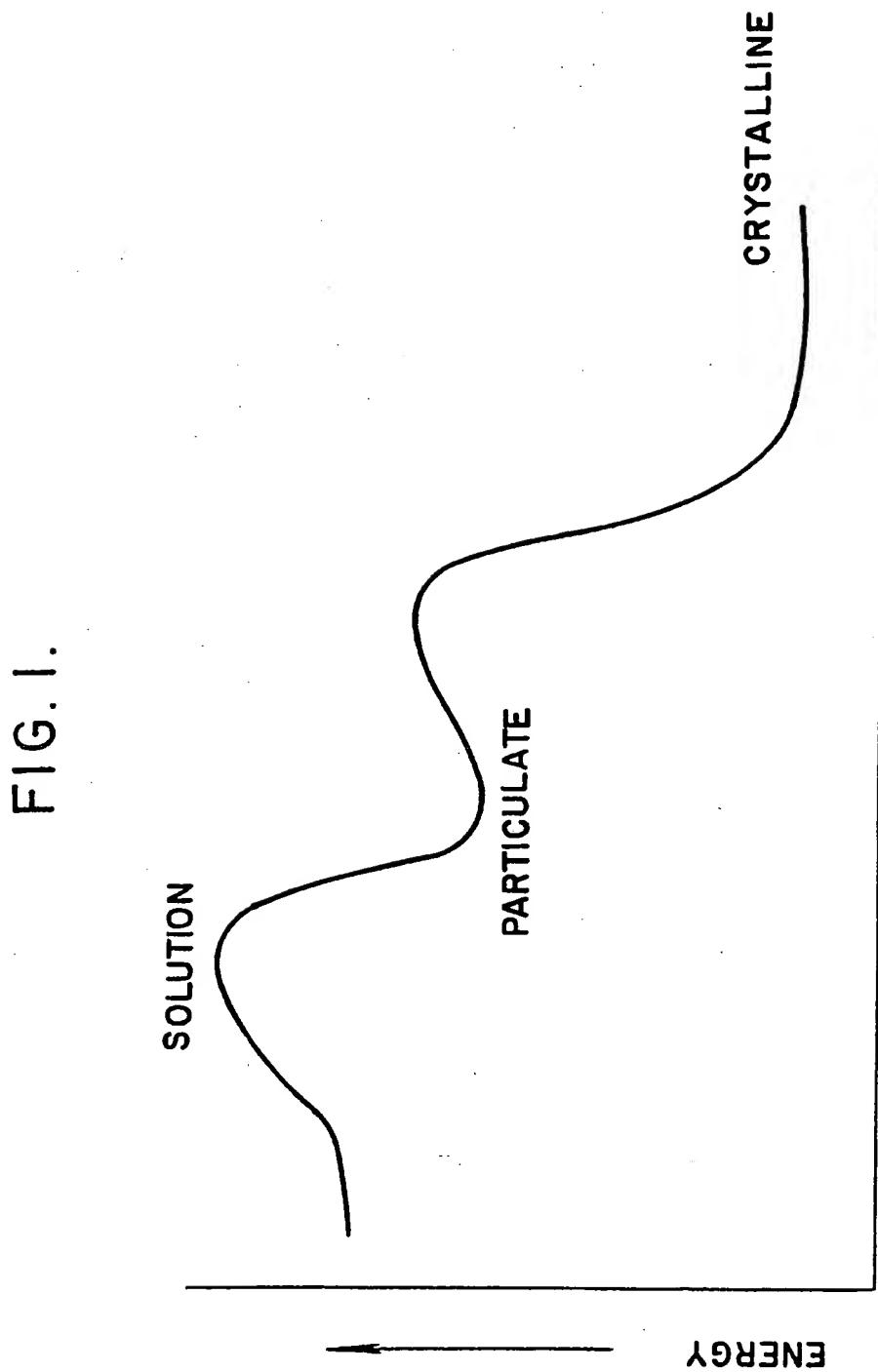
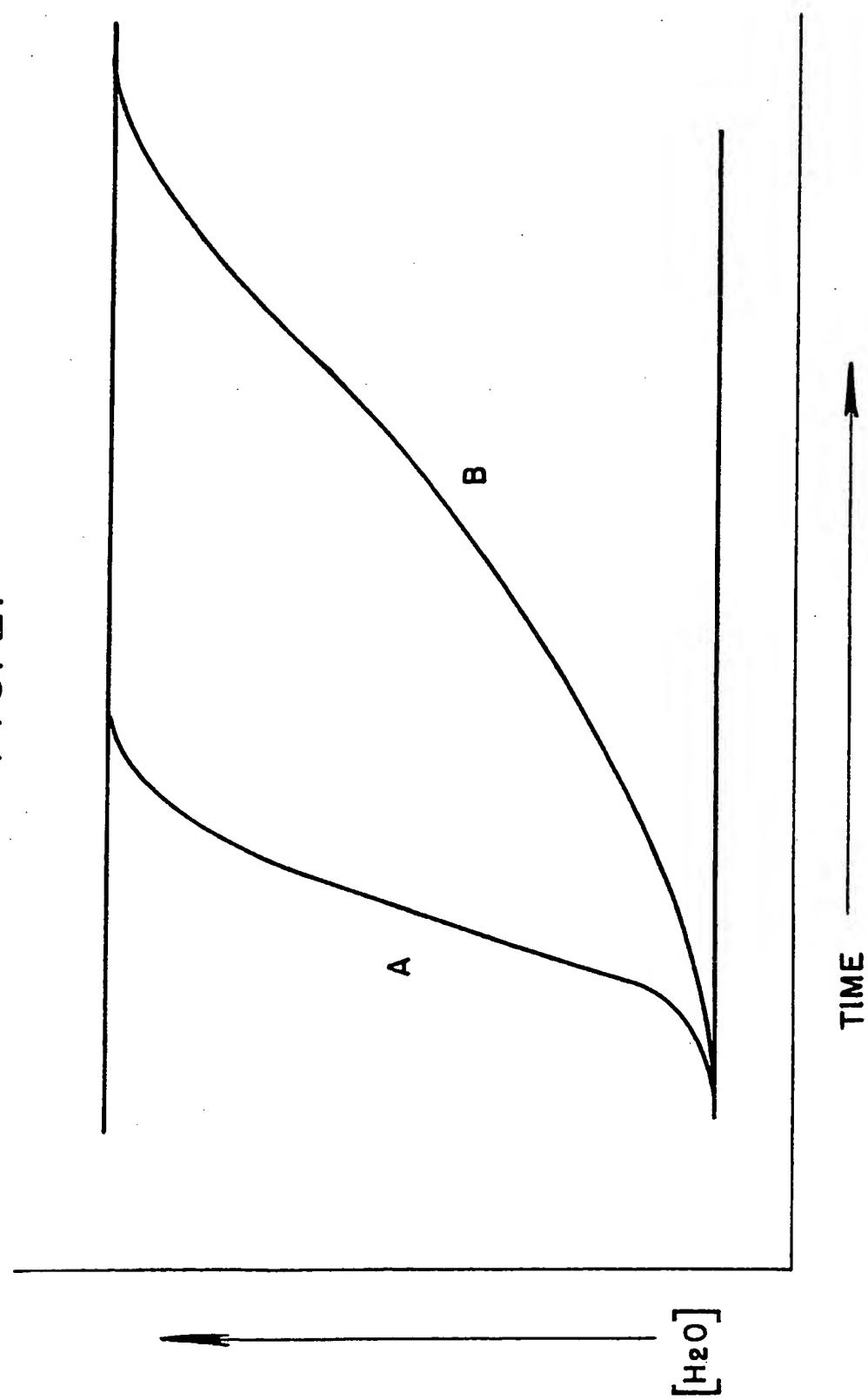


FIG. 2.



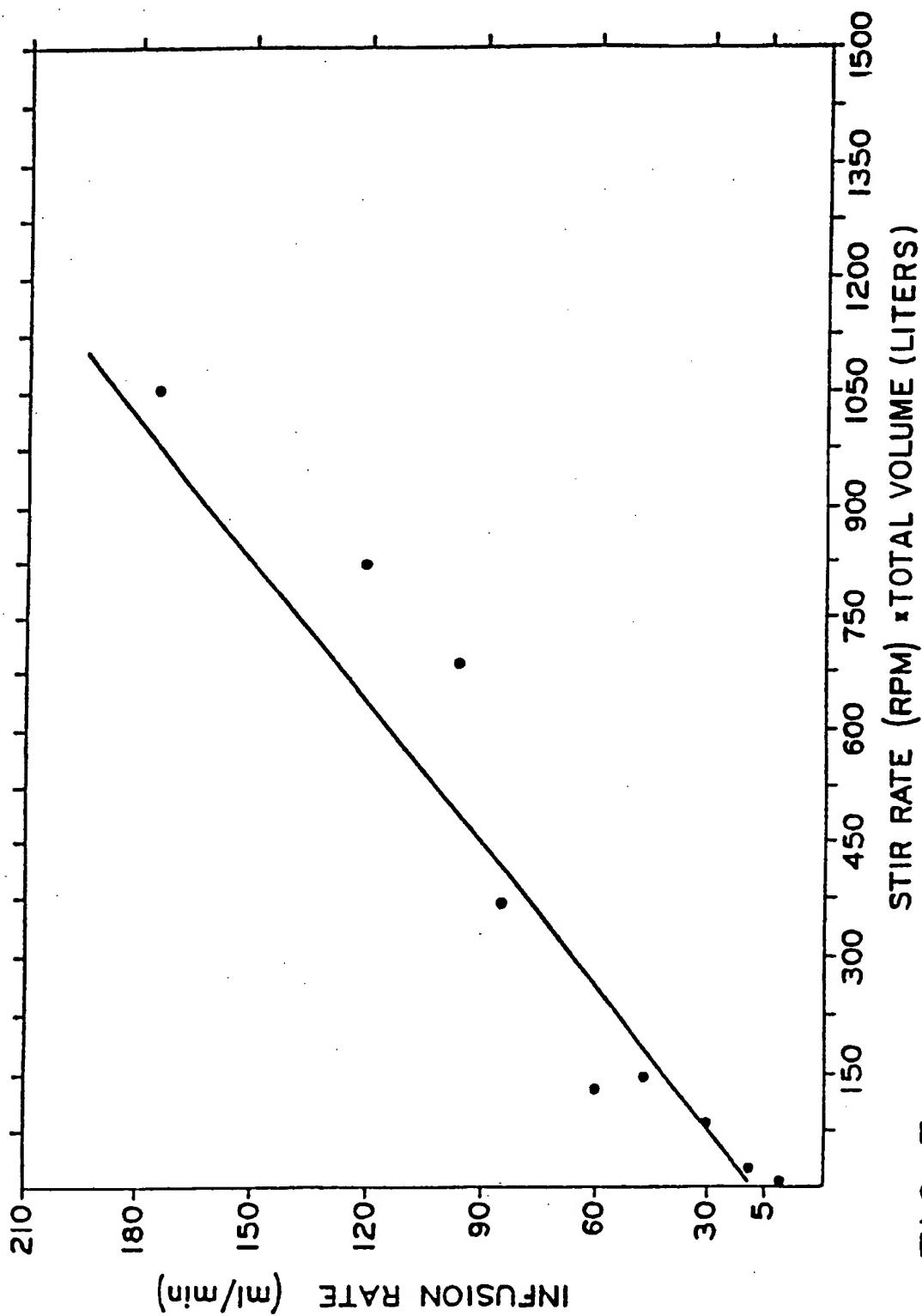


FIG. 3.

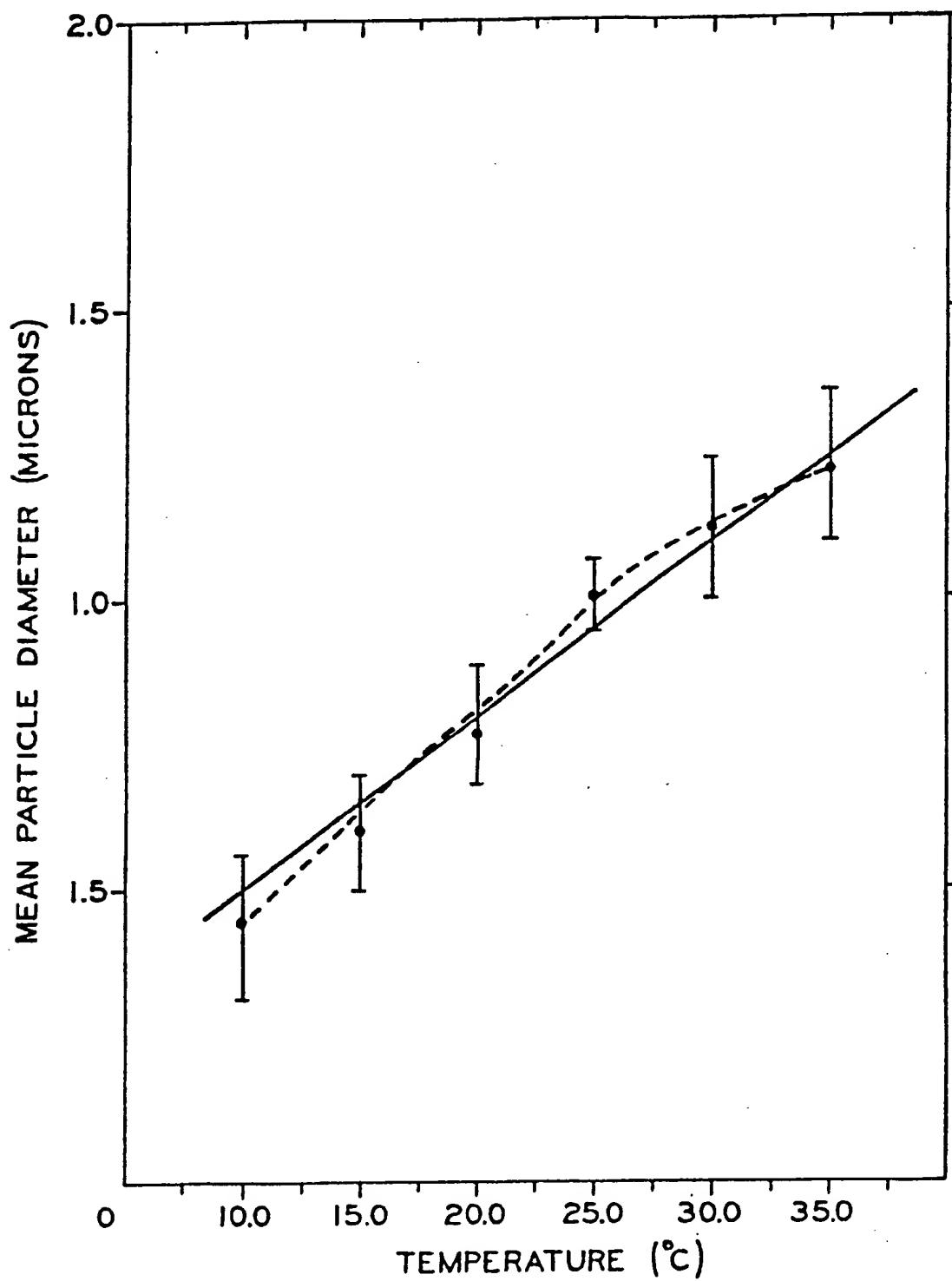
PARTICLE SIZE AS A
FUNCTION OF TEMPERATURE

FIG. 4.

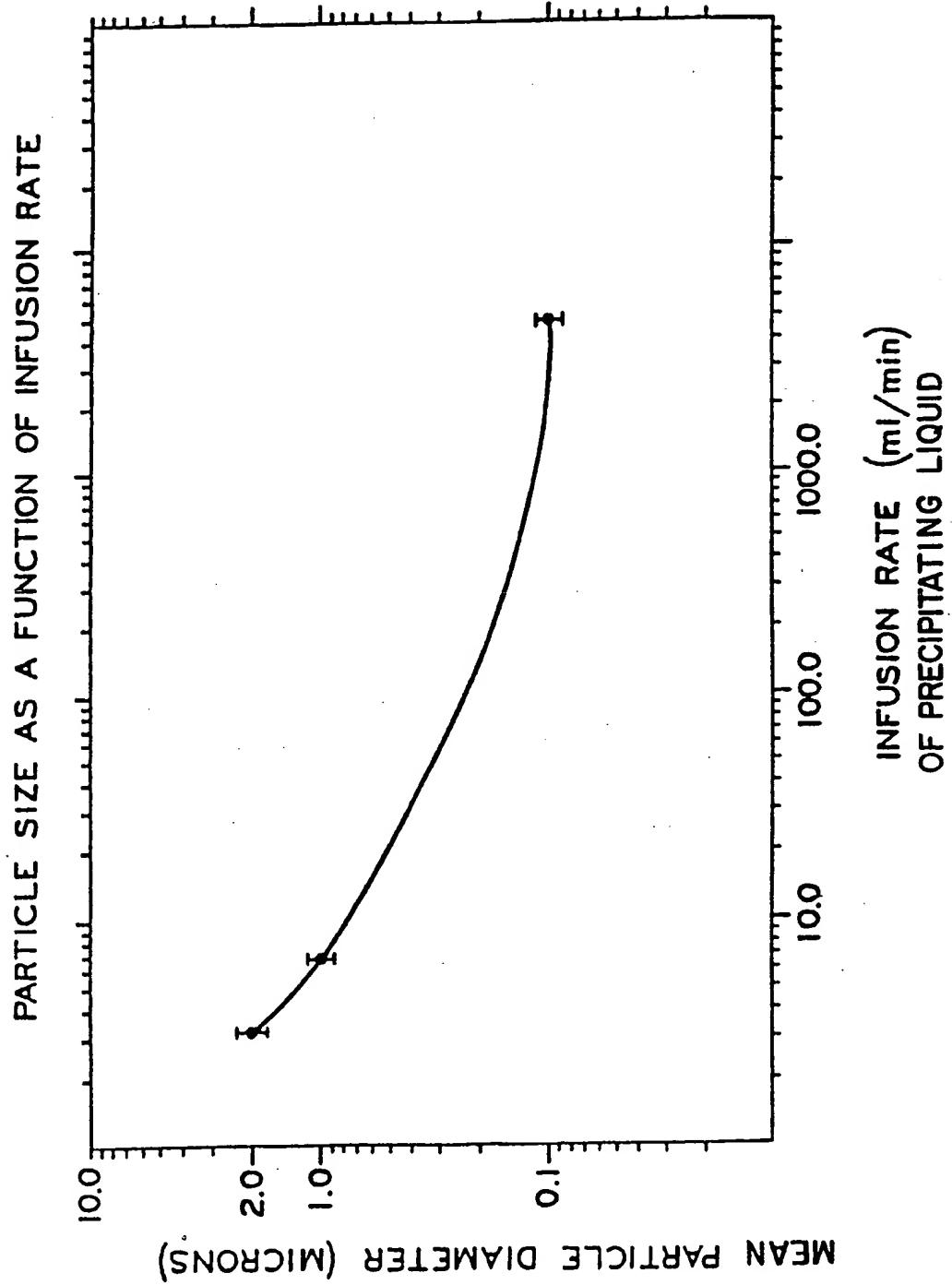


FIG. 5.

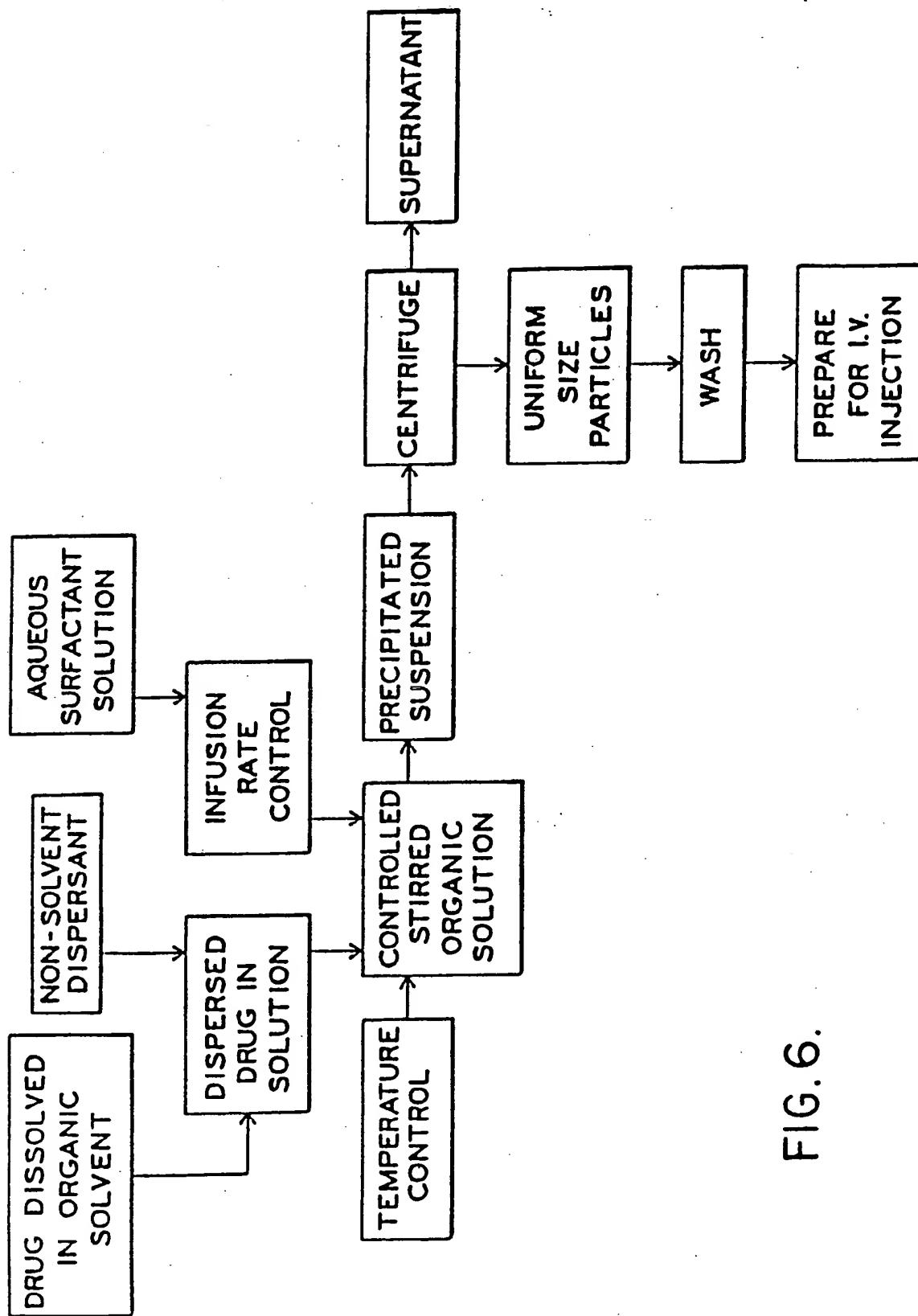


FIG. 6.

INTERNATIONAL SEARCH REPORT

International Application No. PCT/US90/04735

I. CLASSIFICATION OF SUBJECT MATTER (if several classification symbols apply, indicate all) ³

According to International Patent Classification (IPC) or to both National Classification and IPC
IPC(5): C01F 7/34 A61J 37/02
U.S.C.L. 23/305A

II. FIELDS SEARCHED

Minimum Documentation Searched ⁴

Classification System	Classification Symbols
U.S.	23/305A; 210/639,702,709,729,738; 264/9; 423/462,495,605,632; 424/489,490,492,397; 502/8; 514/228.2,410,951,965

Documentation Searched other than Minimum Documentation
to the Extent that such Documents are Included in the Fields Searched ⁵

III. DOCUMENTS CONSIDERED TO BE RELEVANT ¹⁴

Category ⁶	Citation of Document, ¹⁶ with indication, where appropriate, of the relevant passages ¹⁷	Relevant to Claim No. ¹⁸
A	US, A, 4,783,484 (VIOLANTE ET AL) 08 November 1988	1-17
A,&	US, A, 4,826,689 (VIOLANTE ET AL) 02 May 1989 Parent Application of S.N. 342,761.	1-17
A	US, A, 3,887,692 (GILMAN) 03 June 1975	1-7,9,10,12-17
A	US, A, 4,670,461 (HAUGWITZ ET AL) 02 June 1987	1-13
A	US, A, 3,979,520 (ROTHE ET AL) 07 September 1976	1-13

- Special categories of cited documents: ¹⁵
- "A" document defining the general state of the art which is not considered to be of particular relevance
- "E" earlier document but published on or after the international filing date
- "L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)
- "O" document referring to an oral disclosure, use, exhibition or other means
- "P" document published prior to the international filing date but later than the priority date claimed

"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step

"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.

"&" document member of the same patent family

IV. CERTIFICATION

Date of the Actual Completion of the International Search ²

02 NOVEMBER 1990

Date of Mailing of this International Search Report ³

15 FEB 1991

International Searching Authority ¹

ISA/US

Signature of Authorized Officer: **NGUYEN NGOC-HU**
INTERNATIONAL DIVISION

For: **PETER A. HEUSKORI** *Nguyen*